



Dynamic simulation of two CSP concepts with sCO₂ Brayton cycle

1st European Seminar on Supercritical CO₂ (sCO₂) Power Systems Elina Hakkarainen, Teemu Sihvonen, Jari Lappalainen



2

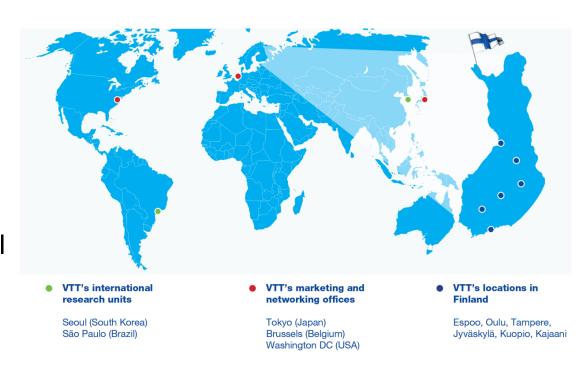
Content

- VTT Technical Research Centre of Finland Ltd
- Background
 - Motivation
 - Scope of the work
 - Simulation environment
- Concepts
 - Concept 1: sCO₂ solar field and power cycle
 - Concept 2: Molten salt solar field and sCO₂ power cycle
- Modelling approach
- Simulation cases
- Simulation results
- Conclusions



VTT Technical Research Centre of Finland Ltd

- Largest multi-technological applied research organization in Northern Europe
- Applied research for needs arising from industry
- Customers are Finnish and international companies as well as public sector organizations
- Total staff over 2,300
- High focus in future low carbon energy systems

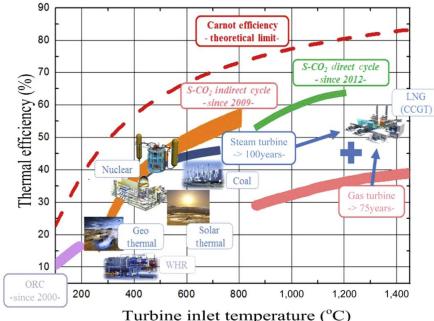


New renewable energy and RES hybrid concepts and distributed energy production



Background: Motivation for the concept development

- New CSP concepts and heat transfer fluids (HTF) needed to improve the efficiency and reduce the levelized cost of electricity
- → One foreseen solution is the introduction of supercritical CO₂ cycles
- Why supercritical carbon dioxide (sCO₂)?
 - Inexpensive, abundant and environmentally friendly
 - Moderate critical pressure and temperature
 - Reduced compression work, high temperatures
 - Smaller component sizes
 - Reduced water consumption in cooling process
- The storage option remains a question
- → Molten salts can provide over night storage solution



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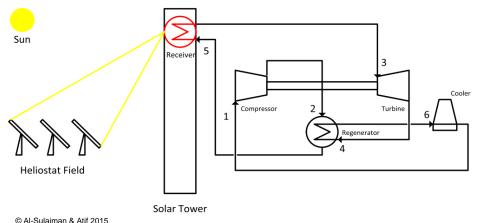


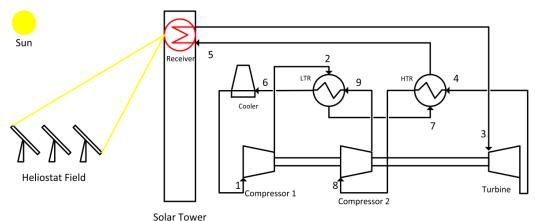
Background: Scope of the work

- 1. To improve dynamic modelling capabilities of sCO₂ CSP plant based on Linear Fresnel Collector (LFC) technology; HTFs, TES, compression modelling etc.
- 2. To introduce a novel LFC concept combining sCO₂ and molten salts for improved efficiency while maintaining dispatchability
- 3. To proof the proper functionality of the models and preliminary control concepts under varying operation modes

Approach in this study:
Regenerative closed loop Brayton cycle

Another possible approach:
Pre-compression closed loop Brayton cycle







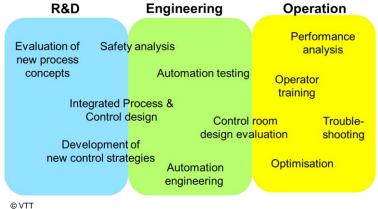
Background: Simulation environment

- Apros[®] is a software package for modelling and dynamic simulation
- Applied for the wide range of processes
 - Nuclear power plants
 - Combustion power plants
 - Pulp & Paper mills
 - General heating and cooling processes
 - Distributed generation & Smart grids
- Developed since 1986 by VTT and Fortum
- Users in 27 countries

Dynamic Simulation Combustion Power Apros features relevant for this study:

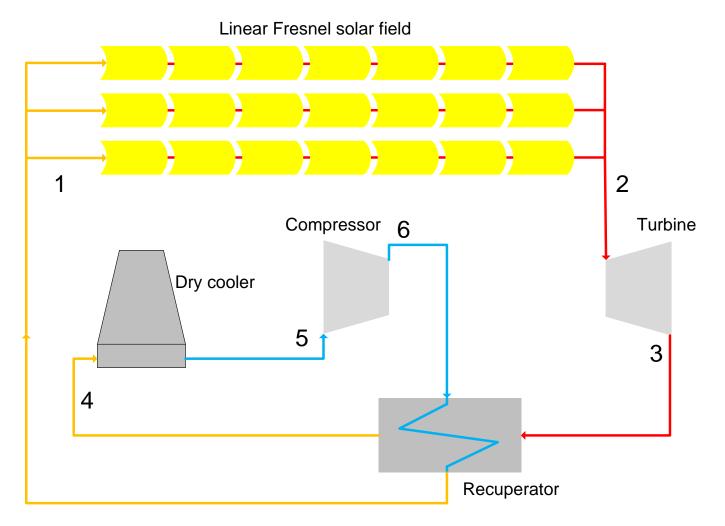
- Accurate process modelling with a set of predefined process components; one-to-one analogous with concrete devices and properly validated
- Sophisticated automation & instrumentation system modelling
- User defined components (User component)
- User definable fluids

Where can be Apros used?





Concept 1: sCO₂ solar field and power cycle





Concept 2: Molten salt solar field and sCO₂ power cycle

Linear Fresnel solar field Cold TES **Hot TES** Solar field inlet pump Compressor Turbine TES pump Dry cooler 6 5 Heat exchanger Recuperator 4



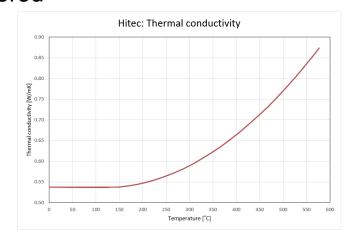
Modelling approach – Heat transfer fluids

Supercritical carbon dioxide (sCO₂)

- Calculation introduced to Apros a few years ago*)
- Calculation based on densely tabulated property data and interpolation by pressure and enthalpy
- CO₂ can exist as liquid, gas or as a two-phase mixture of liquid and vapor
- Air calculation method similar to CO₂
- Homogeneous (3-equation) pressure flow model for all the fluids used

Molten salt: Hitec

- 53% KNO₃+40% NaNO₂+7% NaNO₃
- Freezing point: 142 °C
- Upper temperature limit: 535 °C
- User definable fluid New developments:
 - Air as a non-condensable gas
 - Storage tank simulation possible
- Only the liquid phase of the molten salt is considered

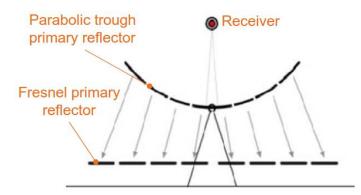




Modelling approach – Solar field

- Linear Fresnel Collectors with vacuum tubes
- Apros User components used for collector modelling
 - Optical behavior
 - Heat transfer
 - Heat losses
- North-South field orientation
- Solar field dimensioned to achieve ~1.2 MW_e power production at design point

| Design point conditions | Concept 1 | Concept 2 |
|---------------------------|-----------|-----------|
| Nr. of collector rows [-] | 3 | 9 |
| Nr. of collectors/row [-] | 7 | 10 |
| Length of the row [m] | 314 | 448 |
| Inlet temperature [°C] | 156 | 280 |
| Outlet temperature [°C] | 350 | 550 |
| Thermal power [MWth] | 5.37 | 22.3 |



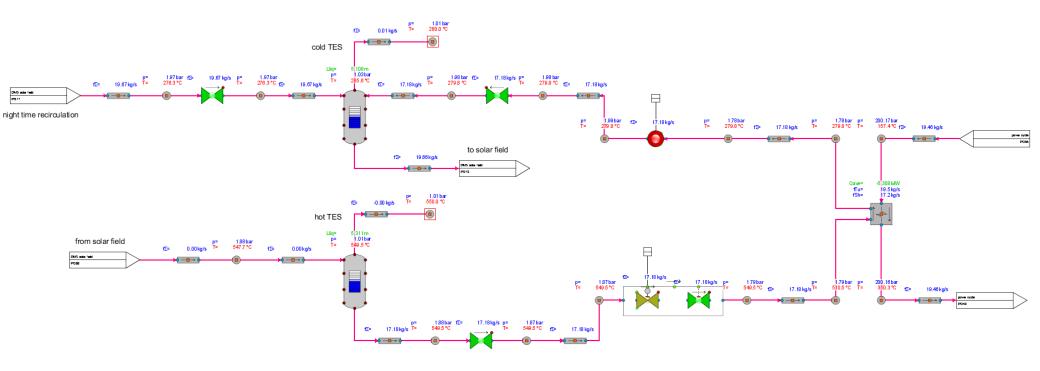


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Modelling approach – Storage system

Two-tank thermal energy storage (TES) system – Only in Concept 2

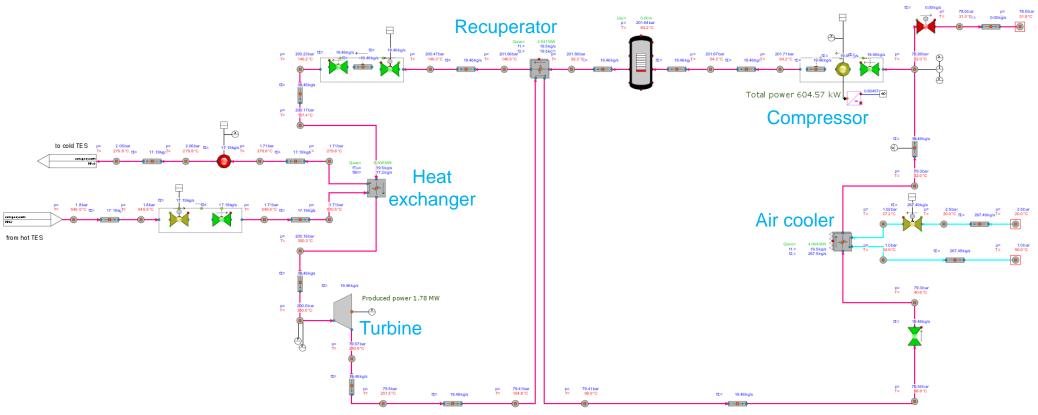




Modelling approach – Power block

Power block model basically similar for both concepts – Different heat source

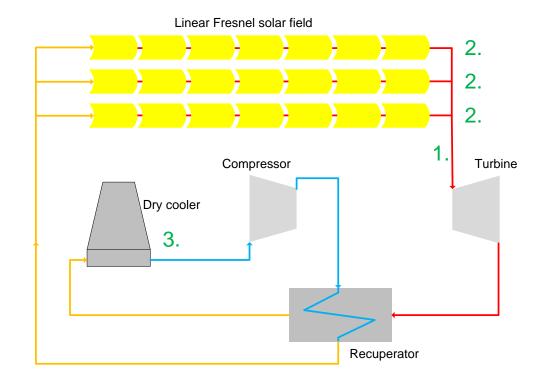
Power block in Concept 2





Modelling approach – Control concept for Concept 1

- 1. Turbine inlet temperature control
 - Through compressor's rotation speed
- Collector row outlet temperature control
 - Through the inlet valve position at the inlet of two first collector rows
- 3. Compressor inlet temperature control
 - Through the cooling air mass flow
- Start-up and shut down modes:
 Minimum speed set point for the compressor

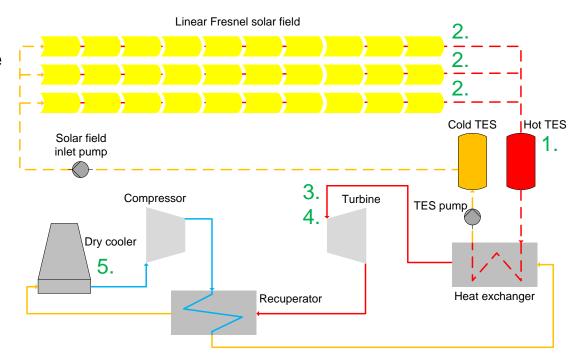




Modelling approach – Control concept for Concept 2

- 1. HE inlet temperature control
 - Through solar field inlet pump's rotation speed
- 2. Collector row outlet temperature control
 - Through the inlet valve position at the inlet of two first collector rows
- 3. Turbine inlet pressure control
 - Through compressor's rotation speed
- 4. Turbine inlet temperature control
 - Through the valve position and TES pump's rotation speed
- Compressor inlet temperature control
 - Through the cooling air mass flow

 Night mode: Molten salt circulation from cold TES through solar field back to cold TES





15

Simulation cases

- Daily performance of two concepts compared with the purpose to
 - Study the sCO₂ heat transfer fluid performance and controllability under varying operation modes
 - Study the molten salt TES operability together with sCO₂ Brayton cycle
 - To compare the daily performance between dispatchable and nondispatchable systems

| Simulation location | Ourzazate, Morocco |
|--------------------------|--------------------------------|
| Latitude | 31.004 °N |
| Longitude | 6.864 °W |
| Simulation date | 21st June i.e. summer solstice |
| Height from see level | 1,143 m |
| Ambient temperature | 25 ℃ |
| *)Turbidity Linke factor | 5.0 |
| *)MOS-corrected DNI | 2,669 kWh/m ² /year |

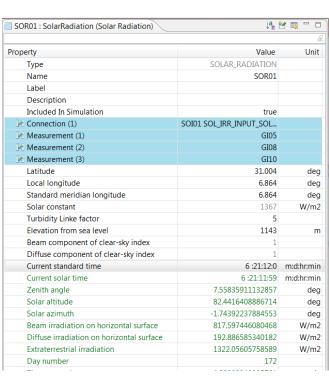


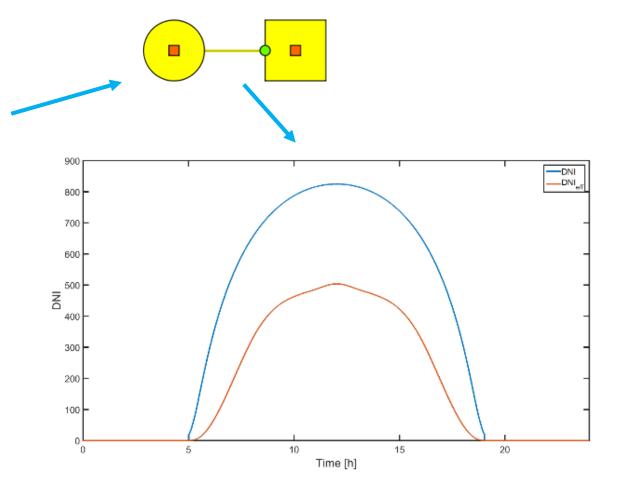


Results: DNI conditions

Clear sky DNI data generated in Apros with Solar Radiation module and Solar Irradiation

Processor module

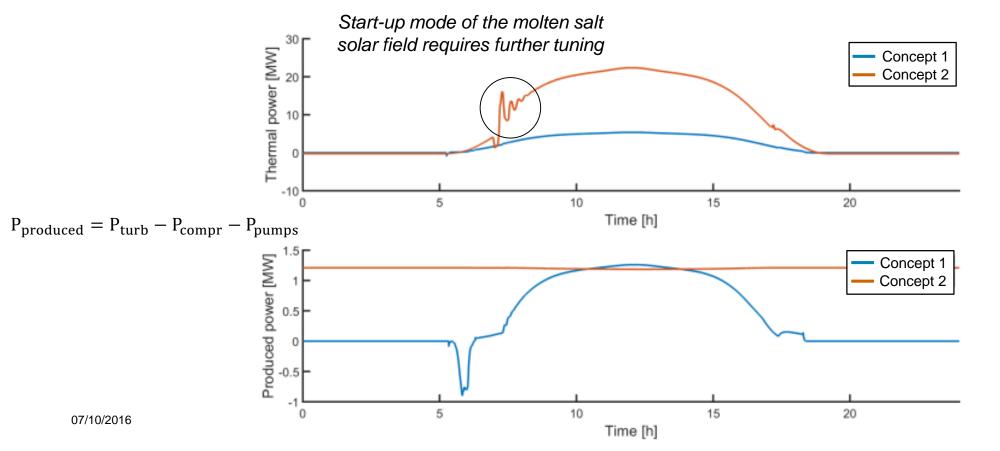






Results: Overall performance

- Produced power follows the load i.e. DNI in Concept 1
- Concept 2 produces constant power due to dispatchability through TES system

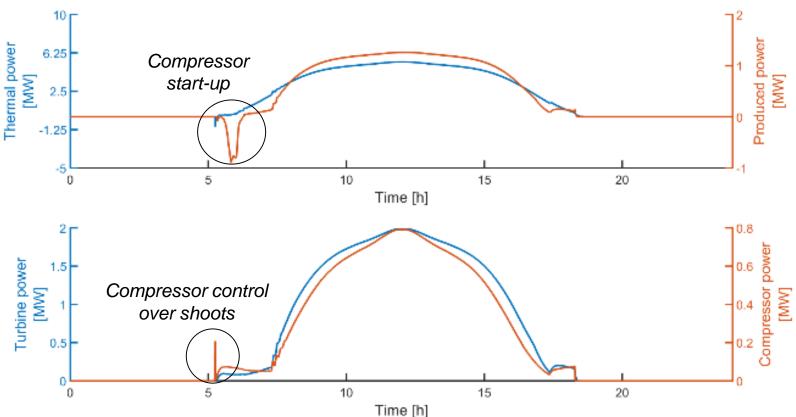




18

Results: Concept 1 thermal performance

Production figures and compressor power consumption follow the DNI trend

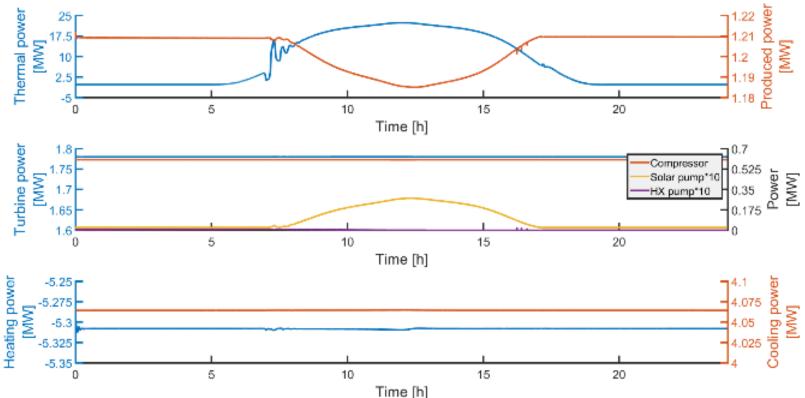




19

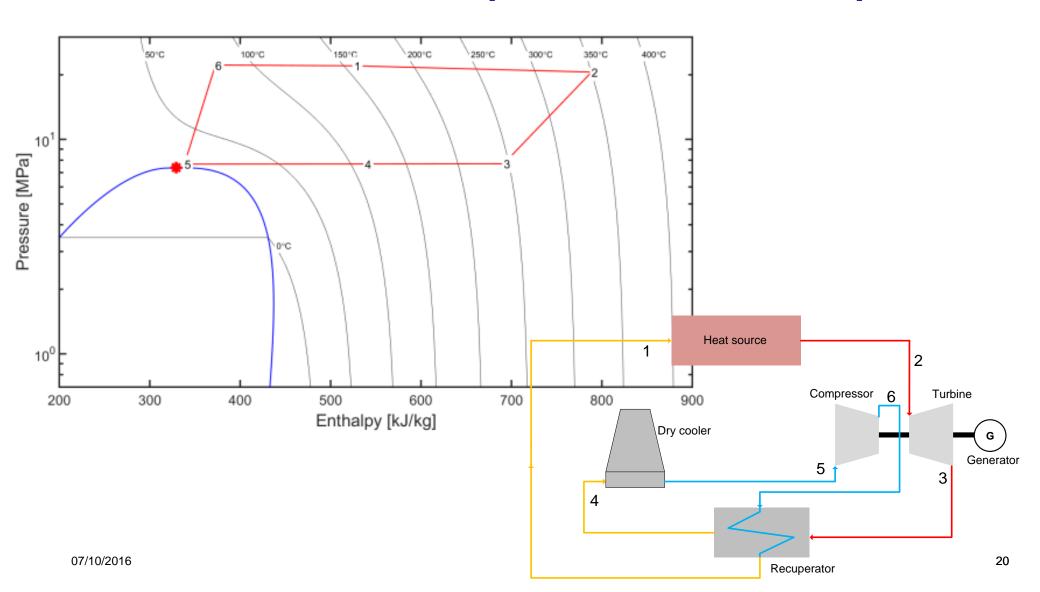
Results: Concept 2 thermal performance

- Constant round the clock turbine power achieved through storage operation
- Produced power not constant due to load-following solar field and HE pumps





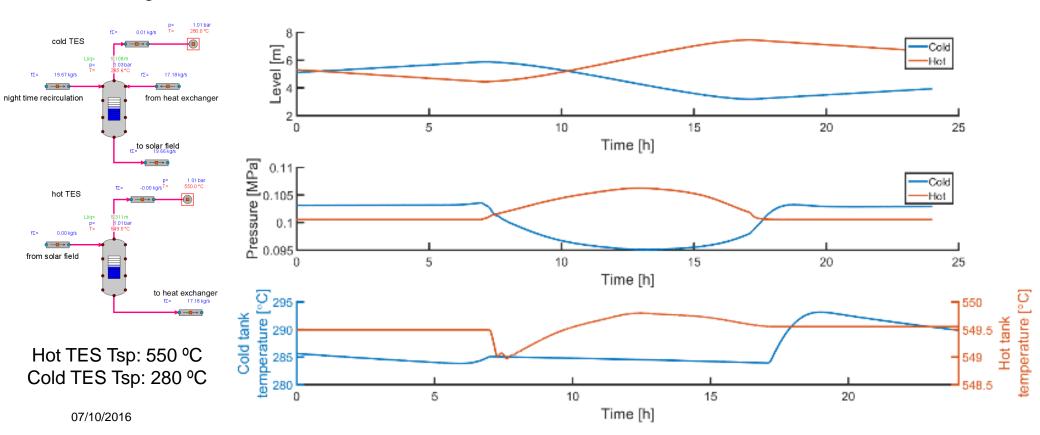
Results: Process state points of both concepts





Results: Storage operations in Concept 2

- In the evening, molten salt accumulated in the hot TES; in the morning, in the cold TES
- The switch between normal operation/night time modes causes minor changes in storage tank temperatures





Results: Concept comparison

- Over 12-fold total solar thermal production is needed by Concept 2 with respect to Concept 1 on June 21st
 - In this case, constant power production → Load following power production
- Produced power by Concept 2 around 3-fold higher with respect to Concept 1
- → Solar multiple 4.2 rather high under design conditions
- During off-design conditions high solar multiple needed
- Higher temperature levels needed to increase the efficiency

| | Concept 1 | Concept 2 |
|------------------------------------|-----------|-----------|
| Produced power [MWh] | 9.6 | 28.9 |
| Thermal energy [MWh] | 14.8 | 186.4 |
| Solar multiple | 1 | 4.2 |
| Thermal efficiency at design point | 0.235 | 0.223 |

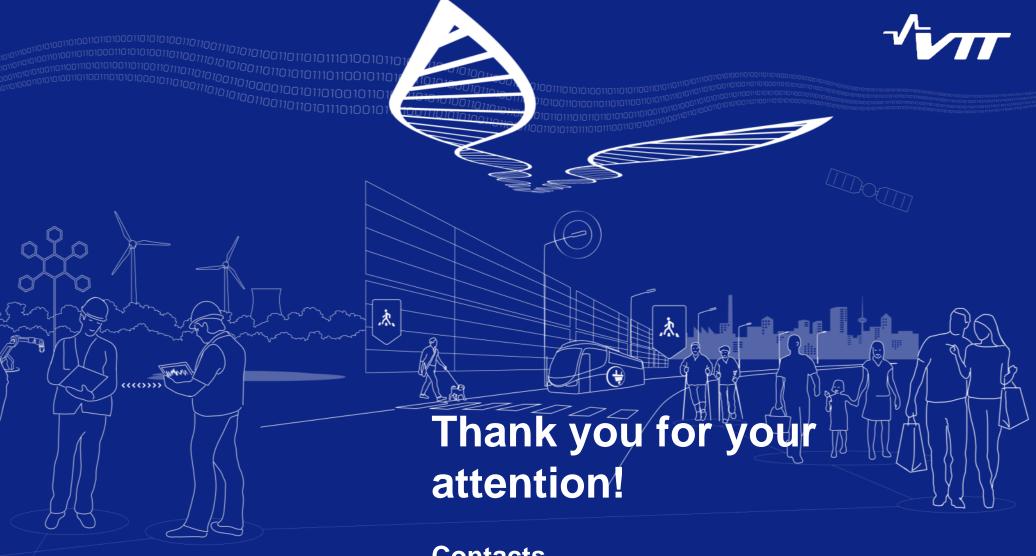
$$\eta_{therm} = \frac{produced\ power}{thermal\ input}$$

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Conclusions

- Overall comparison of the daily behavior of two concepts was given
 - Also details, such as control approaches, start-up and shut down sequences, and component dimensioning, were studied
 - Both concepts looked technically feasible according to detailed dynamic analysis; dispatchability vs. variable production
- To execute a complete comparison between the concepts, yearly performance and economic analyses are needed
 - Local conditions important (need for dispatchability, weather conditions)
 - Detailed behavior under different off-design conditions must be paid attention → An important issue especially in Concept 1
- Future work: Compression work verification, control system development, going into more details in component design
- Apros allows to test and compare also more complex sCO₂ Brayton cycles and analyze the room for efficiency improvements



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